

# REVIEW ON THE PRE-TREATMENT METHODS OF WASTE FOR ANAEROBIC DIGESTION.

Tawsif Hossain Chowdhury<sup>1</sup>

Abstract—Any kind of waste has become a serious threat to society and the environment. Anaerobic digestion process was used in the past primarily to produce biogas. Nowadays the anaerobic digestion process has been widely used in the waste treatment sector because of its high efficiency, better life cycle, and generation of clean energy as an output. However, a great deal of research currently is concentrating on the improvement and optimization of anaerobic digestion under various conditions. The most common process factors such as temperature, pH, volatile fatty acids, hydraulic retention time (HRT), organic loading rate (OLR), etc. are being studied and reviewed in the last few years. But this paper signifies the importance of different types of pre-treatment methods which is the primary and very important step of the anaerobic digestion process. The quality and the efficiency to produce biogas within the required timeframe is largely depended on the proper choice of pre-treatment method among other process parameters. Without applying the specific pretreatment method for an explicit type of waste, the whole digestion cycle can go in the wrong direction. This paper aims to review different pre-treatment methods including mechanical, thermal, and chemical methods for diverse types

**Keywords**—Anaerobic Digestion, Biogas, Pre-Treatment Method, Waste.

## I. INTRODUCTION

THE amount of fossil fuels in the globe is getting limited day by day because of excessive exploitation due to the growth of population, urbanization, industrialization, etc. Therefore, in the last few decades, the use of different renewable sources is receiving attention throughout the globe. Solar, wind, geothermal, hydro, biogas, etc. are the most common forms of renewable energy sources. But among all, biogas probably is one of the promising sources of clean energy as this doesn't have to depend entirely on the availability of other natural sources. For example, solar energy requires sunlight, hydro requires a flow of water or height, wind plant needs a windy environment. Whereas biogas production depends on the availability

T. H. Chowdhury is with the Department of Electrical and Electronic Engineering, Southeast University, 251/1 & 252 Tejgaon I/A, Dhaka 1208, Bangladesh (e-mail: thchowdhury@seu.edu.bd).

of the waste materials either food waste or sewage sludge waste. Biogas is the most versatile energy as it can be converted to heat and/or electricity. Biogas can also be purified to convert into biomethane. Biomethane is suitable to replace fossil natural gas in many applications like electricity production, transportation fuel, etc. [1].

Food waste or sewage sludge waste from humans or animals are the main components of the biogas production process. Wastewater is the mixture of liquid or water-carried wastes from industrial, commercial, and residential along with surface water, groundwater from rain [2]. Wastewater contains undesirable solid contents including organic, inorganic, or toxic substances along with many microorganisms. Sludge is the composition of poorly biodegradable organic compounds and looks like heavily concentrated biomass due to the involvement of physical-chemical processes in the treatment plant. The organic solids comprise proteins, carbohydrates, fats, and oils [3]. The protein contains about 16% nitrogen, and together with urea are the major sources of nitrogen in wastewater [4]. Sludge is rich in nutrients such as nitrogen, phosphorus, etc., and many other valuable organic matters which are very useful for micros during the anaerobic digestion process. Westerhoff et al. [5] reported that if all the substance in sludge could be recovered, it would be worth about US\$13 million annually for a community of 1 million people. The amount of sludge in the world is increasing daily as the population is increasing by around 81 million people per year [6]. Thus it becomes vital to treat this sludge effectively without causing damage to the environment. Many techniques have been used in the past for treating sludge-like composting, pyrolysis and gasification, mono-incineration and cocombustion, hydrothermal methods, etc. But anaerobic digestion (AD) system has been found as one of the most cost-effective and well-implemented technology for waste sludge treatment due to its limited negative environmental impact [7,8]. Anaerobic digestion (AD) is a series of steps where microorganisms break down biodegradable organic materials in a chamber without oxygen to produce biogas and digestate (bio-fertilizer)



[9]. The performance and the growth of microorganisms are sensitive to several operational parameters like pretreatment, temperature, pH, carbon/nitrogen ratio (C/N), type of feedstock, organic loading rate (OLR), hydraulic retention time (HRT), etc. [10]. Proper growth of microbes is essential to improve the production of methane. In this paper, the impact of different pretreatment methods has been reviewed.

# II. ANAEROBIC DIGESTION

The anaerobic digestion process can be defined as the breakdown of complex organic matter by the microorganism without the presence of oxygen to produce methane, carbon dioxide, lower amounts of ammonia, and hydrogen sulfide along with traces of other gasses, such as N<sub>2</sub>, H<sub>2</sub>, CO [14]. The whole process is divided into four phases (hydrolysis, acidogenesis, acetogenesis, and methanogenesis). During the hydrolysis process, the larger molecular weight compounds break into lower molecular weight compounds such as amino acids, fatty acids, and simple sugars [15]. Then in the second phase, organic matters convert into volatile fatty acids. Then the acids convert into acetic acid, hydrogen, and carbon dioxide through acetogenic bacteria which are the major compounds for biogas production. The final methanogenesis step produces methane and carbon dioxide by methanogenic bacteria. Figure 1 shows the breakdown of organic material in different stages of the anaerobic digestion process.

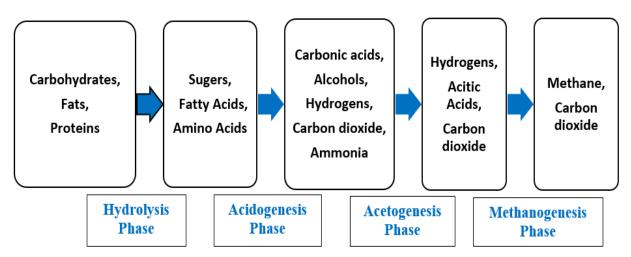


Fig. 1. The key phases of anaerobic digestion [16]

Anaerobic digestion offers huge advantages over aerobic digestion in terms of low energy consumption; reduced solids formation, low nutrient requirements, and better energy recovery. The other alternative treatments like pyrolysis and gasification convert the sludge into fuel whereas incineration and combustion of sludge allow the energy recovery utilizing heat exchangers [11]. All of these sludge treatment methods are much quicker than anaerobic digestion. But they require very a high intensity of energy as input.

# III. PRE-TREATMENTS

Municipal Sludge is the composition of both organic and inorganic materials. Hydrolysis is the rate-limiting step in anaerobic treatment [12]. Pre-treatment before AD helps in accelerating the hydrolysis step and increases further biological mineralization of organic compounds which ultimately improves the biogas yield [13]. Anaerobic digestion without any kind of pretreatment takes more time to complete the whole

digestion process. Various sludge pre-treatment technologies have been proposed, including mechanical, thermal, and chemical treatments to maximize energy recovery [17]. Different methods of pre-treatment have their advantages and impacts on the sludge. Mechanical pre-treatment is already commercially available and can be used in large-scale plants. Mechanical pre-treatment reduces the particle size resulting in an increase in surface area for the microorganisms that will degrade the organic material [18].

# A. Thermal treatment

The thermal treatment process directly breaks the big sludge floc, disruption of cell walls, and degradation of extracellular polymeric substances [19]. It also increases the soluble COD (Chemical Oxygen Demand) concentration and improves dewaterability [20]. However, if the temperature goes higher than 175 °C, the biodegradability of sludge decreases [21]. The improved methane yield was obtained with the



temperatures range between 160 °C and 180 °C (4.8-12.6 bar) for 30-60 min treatment [22, 23, 12, 24, 25]. But it has been found that thermal hydrolysis with high temperature (170-190°C) produces colored recalcitrant compounds (furfurals and 5-hydroxymethylfurfural, phenolic compounds like ferulic acid, syringaldehyde, and vanillin) which slows down the degradation process [26, 27]. Such a reaction is called the Maillard reaction which involves carbohydrates and amino acids [28]. These browning colored compounds have a negative impact on the whole anaerobic system because it increases the dissolved organic nitrogen and high ultraviolet absorbance (UVA254) capacity recalcitrant compounds having a higher molecular weight than 10 kDa with strong color decreases the ultraviolet transmission as this strong brown color increases absorbance (UVA254) capacity [29, 30]. The production of the recalcitrant compound is temperaturedependent, thermal hydrolysis below 160 °C can reduce the probability of creating such browning compounds [31]. The rate of Maillard reaction increases with the temperature. The soluble COD (Chemical Oxygen Demand) and color increase with the temperature ranging between 140-165 °C [21]. The solubilization level of solids increased linearly with the rise of the temperature in treatment [32]. Bougrier et.al. [33] studied the effect of five different types of sludge taken from different plants in south France to explain the solids solubilization. More than 43% solubilization of organic matter has been observed for treatment over 150°C temperatures.

Thermal treatment at 190 °C was found efficient in terms of COD, carbohydrates, proteins and lipid solubility, and methane production. It has been found that carbohydrates had a degradation yield of 82% at 190 °C thermal treatment compared to just 56% without treatment. The degradation rate for protein is just 46% and 35% with or without treatment at the same temperature range. Among these, the degradation of lipid has shown the better result (84%) with 190 °C thermal pre-treatment whereas 67% without treatment. Above all, the methane yield was increased by 25% with 190 °C treatment [32]. But it is required to find out a favorable temperature for treating sludge where there will be fewer melanoidins formed. An optimum temperature of 140 °C has been found for thermal hydrolysis where no significant negative impact has been noticed in terms of biodegradability of the sludge and solubilization of COD [21]. Table I shows the observations of the AD process after thermal pretreatment at different temperatures.

TABLE I
SUMMARY OF KEY RESEARCH ON ANAEROBIC DIGESTION AND
PRE-TREATMENT METHODS

Feedstock/ Input/Fuel Type	Treatment Method	Observation/Outcome	Referen ce
Waste activated sludge and inoculum sludge	Thermal pre- and inter-stage treatment at moderate temperature: at 80° C and high temperature at 130–170° C	Total volatile solid increased from 2 to 29% for thermal treatment. TVS increased from 2 to 27% for inter-stage treatment (80°C). TVS increased from 2 to 25% and 57% at 130 °C and 170 °C respectively with 9% and 29% increase in methane yield.	[34]
Sludge	Thermal pretreatment at 70°C temperature	Has a decisive effect on pathogen removal	[35]
Sludge	pre-treatment at 90°C	Biogas production was improved 20 times when applying a 60 min	[36]

## B. Chemical treatment

In chemical treatment, the cell wall and membrane get hydrolyzed which improves the solubility of organic matter (sludge). The most common chemical treatments are alkali pre-treatments (alkaline hydrolysis and alkaline peroxide), pre-treatment with ozone (ozonolysis), acid hydrolysis treatment (H<sub>2</sub>SO<sub>4</sub>) [37]. The physical and biochemical characteristics of sludge will change with the addition of such chemicals during the pre-treatment step. At first, EPS the extracellular polymeric substances which are located outside the microbial cells gets damaged in the alkaline pretreatment process [38].

**EPS** include proteins, carbohydrates, humic substances, lipids, and nucleic acids [38]. Sodium hydroxide (NaOH), potassium hydroxide (KOH), lime (Ca(OH)<sub>2</sub>), aqueous ammonia (NH<sub>3</sub>·H<sub>2</sub>O), and hydrogen peroxide (H2O2) are reported chemicals that are used in alkaline pre-treatment [39]. Hydroxyl anions destroy the floc structures and cell walls of microorganisms during alkaline treatment. Ionization of hydroxyl groups (OH- $\rightarrow$  -O $^{-}$ ) causes extensive swelling and solubilization of gels in sludge [40]. The destruction of extracellular polymer substances and cell walls results in releasing intracellular substances due to high pH [41]. 63% COD solubilization was achieved and total solids reduction reached 33% with the addition of 21.6g of NaOH/I [42]. Both at ambient and high temperature (140 °C), pretreatment with NaOH and KOH showed better COD solubilization of 71.6% and 83.7% respectively as compared to the dibasic alkali agents (Mg(OH)<sub>2</sub>, Ca(OH)<sub>2</sub>) [42]. The thermal or ultrasonic alkaline process had better results in reducing particle size compared to thermal or ultrasonic-acid pretreatment



[43]. Sulphuric acids (H<sub>2</sub>SO<sub>4</sub>), hydrochloric acid (HCl), acetic acid (CH<sub>3</sub>COOH) are the acid chemicals that are commonly used in acid hydrolysis [44].

# C. Ozone treatment

Ozone has been used as part of pretreatment because of its strong oxidative properties. 25% improvement in methane production was achieved by Erden and Filibeli [45] when the secondary sludge had been pre-treated by ozone. During sludge ozonation, ozone decomposes itself into radicals and reacts with soluble and particular fractions, organic or mineral fractions. Ozonation improves the viscosity and settlement of sludge [46]. Compared to raw sludge, ozonated sludge at 0.1 g O<sub>3</sub>/g-SS for 5 days showed 2-3 times greater biodegradability [47]. An optimal range for ozone dose has been reported from 0.05 to 0.5 g  $O_3/g$  of total solid [48]. The TVS removal efficiency was increased by 35-90% when sludge was pre-treated with ozone [49]. Ozone dose of 0.15 g O<sub>3</sub>/g total solids showed an increase in SCOD (Soluble chemical oxygen demand) up to 37% along with improvement in the biogas yield around 2.4 times greater than control [48]. However higher ozone dose can lead to the formation of by-products that are less biodegradable [50]. Higher doses of ozonation (higher than 0.18 g O<sub>3</sub>/g TS) can lead to a mineralization phenomenon. Performance decreases with a higher dose probably due to the inappropriate acidic environment inside the digester or the formation of recalcitrant ozonation as by-products [48]. Other downsides of the ozonation process are foaming and poorer filterability of treated sludge [46]. Table II shows the results of the AD process after ozone pre-treatment.

TABLE II
SUMMARY OF KEY RESEARCH ON ANAEROBIC DIGESTION AND
PRE-TREATMENT METHODS

THE THE THE THE THE THE THE							
Feedstock/ Input/Fuel Type	Reactor Type	Treatment Method	Observation/ Outcome	Refere nce			
Waste activated sludge and inoculum sludge	Batch reactor for 40 days	Thermal preand interstage treatment at moderate temperature: at 80° C and high temperature at 130–170° C	57% at 130 C and 170 °C respectively with a 9% and 29% increase in	[34]			
			methane yield.	l			

Feedstock/ Input/Fuel Type	Reactor Type	Treatment Method	Observation/ Outcome	Refere nce
Mixed sludge	-	Thermal hydrolysis pre-treatment at 150–170°C, 4.8–7.9 bar.	56–62% reduction in volatile solid in digestate. 24–59% increase in biogas production	[25]
Primary, Secondary and mixed sludge	A semi- continuous reactor at 30 days SRT at 35°C	Thermal pretreatment using hydrolyser at 134–140°C, 3.4 bar for 30 min.	12.6% reduction in volatile solid in digestate. 40.2% increase in methane production	[51]
Dewatered sludge (high solid sludge)	A batch reactor at 28 days SRT at 37°C	Thermal pretreatment using low-temperature hydrolysis at 60–90°C, for 1–72 h	557–1678% increase in SCOD (Soluble chemical oxygen demand)	[52]

## IV. CONCLUSION

The anaerobic digestion process has demonstrated its potential as a technology that not only can reduce the waste amount but also can be used for the production of renewable heat and power and compost. Among all kinds of treatment processes. The thermal treatment process is the most popular method despite having high energy requirements and the potential to produce ammonia and recalcitrant compounds due to overheating. But this process helps to reduce the total volume of waste and reduce the pathogens. On the other hand, despite being expensive and toxic, the chemical process improves the solubility of waste and boosts the methane yield. The combination of two or more types of pretreatment methods still requires much attention despite being costly. Therefore, more study is required to identify the optimized set of parameters for full-scale which could improve the methane production along with the reduction in cost and time.

## REFERENCES

- R. Wirth et al., "Characterization of a biogas-producing microbial community by short-read next-generation DNA sequencing." Biotechnology for biofuels, vol. 5, no. 1, pp. 1-16, 2012. DOI: https://doi.org/10.1186/1754-6834-5-41
- [2] O.F. A. Ibiam, and I. Ifeanyi, "Sewage management and its benefits to man." *International Research Journal of Biotechnology* Volume 3, Issue 10, pp. 174 – 189, 2012.
- [3] K.D. Monson et al., "Anaerobic digestion of biodegradable municipal wastes: a review." *University of Glamorgan ISBN*, pp.978-971, 2007.
- [4] Westgate, Pamela J., and Chul Park. "Evaluation of proteins and organic nitrogen in wastewater treatment effluents." Environmental science & technology, vol. 44, no. 14, 5352-5357, 2010.



- [5] Westerhoff, Paul, Sungyun Lee, Yu Yang, Gwyneth W. Gordon, Kiril Hristovski, Rolf U. Halden, and Pierre Herckes. "Characterization, recovery opportunities, and valuation of metals in municipal sludges from US wastewater treatment plants nationwide." *Environmental science & technology*, vol. 49, no. 16, pp. 9479-9488, 2015. DOI: https://doi.org/10.1021/es505329q
- [6] Worldometer, 2020. Current World Population. https://www.worldometers.info/world-population/#:~:text=Population%20in%20the%20world%20is,it%20was%20at%20around%202%25. (accessed 10 August 2020).
- [7] Zhao, Ting, Yongdong Chen, Qing Yu, Dezhi Shi, Hongxiang Chai, Li Li, Hainan Ai, Li Gu, and Qiang He. "Enhancement of performance and stability of anaerobic co-digestion of waste activated sludge and kitchen waste by using bentonite." *PloS one*, vol. 14, no. 7, e0218856, 2019. DOI: https://doi.org/10.1371/journal.pone.0218856
- [8] F.V. Carstensen et al., "New and Future Developments in Catalysis: Chapter 13. "Economic Analysis of Bioenergy: An Integrated Multidisciplinary Approach. Elsevier Inc. 2013.
- [9] T.H. Chowdhury, "Technical-economical analysis of anaerobic digestion process to produce clean energy." *Energy Reports*, vol. 7, pp.247-253, 2021.
- [10] R.A. Labatut, and J.L. Pronto, "Sustainable Waste-to-Energy Technologies: Anaerobic Digestion." In Sustainable Food Waste-To-energy Systems (pp. 47-67). Academic Press, 2018.
- [11] O. Suárez-Iglesias et al., "Valuable compounds from sewage sludge by thermal hydrolysis and wet oxidation. A review." Science of the Total Environment, 484-585, pp. 921-934, 2017. DOI: https://doi.org/10.1016/j.scitotenv.2017.01.140
- [12] Y.Y. Li, and T. Noike, "Upgrading of anaerobic digestion of waste activated sludge by thermal pretreatment." Water Science and Technology, 26(3-4), pp.857-866, 1992.
- [13] E. Wiśniowska, "Sludge activation, conditioning, and engineering. In Industrial and Municipal Sludge" (pp. 181-199). Butterworth-Heinemann, 2019. DOI: https://doi.org/10.1016/B978-0-12-815907-1.00009-X
- [14] M. Taherzadeh et al. "Sustainable resource recovery and zero waste approaches", Elsevier, 2019.
- [15] T. Letcher, "Comprehensive renewable energy." Newnes. 2012.
- [16] K.F. Adekunle, and J.A. Okolie, "A review of biochemical process of anaerobic digestion," *Advances in Bioscience and Biotechnology*, 6(03), pp.205-212, 2015. DOI: https://doi.org/10.4236/abb.2015.63020
- [17] W. Wei et al., "Free ammonia pre-treatment of secondary sludge significantly increases anaerobic methane production." Water research, 118, pp.12-19. 2017. DOI: https://doi.org/10.1016/j.watres.2017.04.015
- [18] J. Lindmark et al., "Effects of mechanical pre-treatment on the biogas yield from ley crop silage." Applied Energy, vol. 97, pp.498-502, 2012. DOI: https://doi.org/10.1016/j.apenergy.2011.12.066
- [19] M.P. Weemaes, and W.H. Verstraete, "Evaluation of current wet sludge disintegration techniques." Journal of Chemical Technology & Biotechnology: International Research in Process, Environmental AND Clean Technology, vol. 73. no. 2, pp.83-92, 1998. DOI: https://doi.org/10.1002/(SICI)1097-4660(1998100)73:2<83::AID-JCTB932>3.0.CO;2-2
- [20] A. Mottet et al., "Kinetics of thermophilic batch anaerobic digestion of thermal hydrolysed waste activated sludge." Biochemical Engineering Journal, vol. 46, no. 2, pp.169-175, 2009. DOI: https://doi.org/10.1016/j.bej.2009.05.003
- [21] J. Dwyer et al., "Decreasing activated sludge thermal hydrolysis temperature reduces product colour, without decreasing degradability." Water research, vol. 42, no. 18, pp.4699-4709, 2008. DOI: https://doi.org/10.1016/j.watres.2008.08.019
- [22] R.T. Haug et al., "Effect of thermal pretreatment on digestibility and dewaterability of organic sludges." *Journal (Water Pollution Control Federation)*, pp.73-85, 1978.

- [23] D.C. Stuckey, and P.L. McCARTY, "Thermochemical pretreatment of nitrogenous materials to increase methane yield." *Biotechnol. Bioeng. Symp.*; (United States) (Vol. 8). Stanford Univ., CA. 1978
- [24] S. Tanaka et al., "Effects of thermochemical pretreatment on the anaerobic digestion of waste activated sludge." Water Science and Technology, vol. 35, no. 8, pp.209-215, 1997. DOI: https://doi.org/10.2166/wst.1997.0315
- [25] C.A. Wilson et al., "Anaerobic digestion of raw and thermally hydrolyzed wastewater solids under various operational conditions." Water Environment Research, vol. 83, no. 9, pp.815-825, 2011.
- [26] B. Ahmed et al., "Improvement of anaerobic digestion of lignocellulosic biomass by hydrothermal pretreatment." Applied Sciences, vol. 9, no. 18, pp.3853, 2019.
- [27] R. Lin et al., "Inhibitory effects of furan derivatives and phenolic compounds on dark hydrogen fermentation." Bioresource technology, vol. 196, pp.250-255., 2015.
- [28] H. Carrère et al., "Pretreatment methods to improve sludge anaerobic degradability: a review." Journal of hazardous materials, vol. 183, no. 1-3, pp.1-15, 2010. DOI: https://doi.org/10.1016/j.jhazmat.2010.06.129
- [29] J. M. Abelleira-Pereira et al., "Enhancement of methane production in mesophilic anaerobic digestion of secondary sewage sludge by advanced thermal hydrolysis pretreatment." Water research, 71, pp.330-340. 2015. DOI: https://doi.org/10.1016/j.watres.2014.12.027
- [30] O.K. Svennevik et al., "Quantification of soluble recalcitrant compounds in commercial thermal hydrolysis digestates." Water Environment Research. 2020
- [31] M. Corzo-Martinez et al., "Chapter 4. Browning reactions. In: Hui, Y.H., Nip, W.-.K., Nollet, L.M.L., Paliyath, G., Simpson, B.K. (Ed.)." Food Biochemistry and Food Processing. Wiley-Blackwell, pp. 83e85, 2006.
- [32] H. Carrère, Bougrier et al., "Impact of initial biodegradability on sludge anaerobic digestion enhancement by thermal pretreatment." Journal of Environmental Science and Health Part A, vol. 43, no. 13, pp.1551-1555, 2008. DOI: https://doi.org/10.1080/10934520802293735
- [33] C. Bougrier, J.P. Delgenes, J.P. and H. Carrère, "Effects of thermal treatments on five different waste activated sludge samples solubilisation, physical properties and anaerobic digestion." *Chemical Engineering Journal*, vol. 139, no. 2, pp.236-244, 2008. https://doi.org/10.1016/j.cej.2007.07.099
- [34] H.B. Nielsen et al., "Anaerobic digestion of waste activated sludge—comparison of thermal pretreatments with thermal inter-stage treatments. Journal of Chemical Technology & Biotechnology, vol. 86, no. 2, pp.238-245, 2011.
- [35] I.V. Skiadas et al., "Thermal pre-treatment of primary and secondary sludge at 70 C prior to anaerobic digestion." Water Science and Technology, vol. 52, no. 1-2, pp.161-166, 2005
- [36] L. Appels et al., "Influence of low temperature thermal pretreatment on sludge solubilisation, heavy metal release and anaerobic digestion." Bioresource technology, vol. 101, no. 15, pp.5743-5748, 2010.
- [37] A. Mudhoo, "Biogas production: pretreatment methods in anaerobic digestion." John Wiley & Sons, 2012.
- [38] B. Xiao et al., "Evaluation of the microbial cell structure damages in alkaline pretreatment of waste activated sludge." Bioresource technology, 196, pp.109-115, 2015. DOI: https://doi.org/10.1016/j.biortech.2015.07.056
- [39] G. González et al., "Protein hydrolysis under anaerobic, saline conditions in presence of acetic acid." Journal of Chemical Technology & Biotechnology: International Research in Process, Environmental & Clean Technology, vol. 80, no. 2, pp.151-157, 2005. DOI: https://doi.org/10.1002/jctb.1165
- [40] E. Neyens, J. Baeyens, and R. Dewil, "Advanced sludge treatment affects extracellular polymeric substances to improve activated sludge dewatering." *Journal of hazardous materials*,



- vol. 106, no. 2-3, pp.83-92, 2004. DOI: https://doi.org/10.1016/j.jhazmat.2003.11.014
- [41] J.I.N. Yiying et al., "Combined alkaline and ultrasonic pretreatment of sludge before aerobic digestion." Journal of Environmental Sciences, vol. 21, no. 3, pp.279-284, 2009. https://doi.org/10.1016/S1001-0742(0862264-0
- [42] V. Penaud, J.P. Delgenes, and R. Moletta, "Thermo-chemical pretreatment of a microbial biomass: influence of sodium hydroxide addition on solubilization and anaerobic biodegradability." Enzyme and microbial technology, vol. 25, no. 3, pp.258-263, 1999. DOI: <a href="https://doi.org/10.1016/S0141-0229(9900037-X">https://doi.org/10.1016/S0141-0229(9900037-X</a>
- [43] X. Liu et al., "Enhancement of solubilization and acidification of waste activated sludge by pretreatment." Waste Management, vol. 28, no. 12, pp.2614-2622, 2008. https://doi.org/10.1016/j.wasman.2008.02.001
- [44] F.R. Amin et al., "Pretreatment methods of lignocellulosic biomass for anaerobic digestion." Amb Express, vol. 7. No. 1, pp.72, 2017. DOI: https://doi.org/10.1186/s13568-017-0375-4
- [45] G. Erden, and A. Filibeli, "Ozone oxidation of biological sludge: Effects on disintegration, anaerobic biodegradability, and filterability." *Environmental Progress & Sustainable Energy*, vol. 30, no. 3, 377-383, 2011. DOI: https://doi.org/10.1016/j.mib.2005.04.011
- [46] A. Battimelli et al., "Anaerobic digestion of waste activated sludge combined with ozone post-treatment and recycling." Water science and technology, vol. 48, no. 4, pp.61-68, 2003. DOI: https://doi.org/10.2166/wst.2003.0222
- [47] I.T. Yeom et al., "Effects of ozone treatment on the biodegradability of sludge from municipal wastewater treatment plants." Water Science and Technology, vol. 46, no. 4-5, pp.421-425, 2002. DOI: https://doi.org/10.2166/wst.2002.0641
- [48] C. Bougrier et al., "Combined ozone pretreatment and anaerobic digestion for the reduction of biological sludge production in wastewater treatment." Ozone: Science and Engineering, vol. 29, no. 3, pp.201-206, 2007. DOI: <a href="https://doi.org/10.1080/01919510701296754">https://doi.org/10.1080/01919510701296754</a>
- [49] R. Goel, T. Tokutomi and H. Yasui, "Anaerobic digestion of excess activated sludge with ozone pretreatment." Water science and technology, vol. 47, no. 12, pp.207-214, 2003. DOI: https://doi.org/10.2166/wst.2003.0648
- [50] A. Cesaro and V. Belgiorno, "Sonolysis and ozonation as pretreatment for anaerobic digestion of solid organic waste."

- *Ultrasonics sonochemistry*, vol. 20. no. 3, pp.931-936, 2013. DOI: https://doi.org/10.1016/j.ultsonch.2012.10.017
- [51] S. Pilli et al., "Ultrasonic pretreatment of sludge: a review." Ultrasonics sonochemistry, vol. 18, no. 1, pp.1-18, 2011. DOI: https://doi.org/10.1016/j.ultsonch.2010.02.014
- [52] Y. Xue et al., "Effects of thermal hydrolysis on organic matter solubilization and anaerobic digestion of high solid sludge." Chemical Engineering Journal, vol. 264, pp.174-180, 2015.



Tawsif Hossain Chowdhury was born in Dhaka, Bangladesh on 17 December 1988. He received the BSc. degree in Electrical and Electronic Engineering from American International University Bangladesh (AIUB) in 2012. In 2017, he completed his MSc. degree

in Renewable Energy and Resource Management from the University of South Wales, the UK under the Commonwealth Shared Scholarship. Currently, he is working as a lecturer in the Department of Electrical and Electronic Engineering of Southeast University, Dhaka, Bangladesh. Previously, he worked at Robi Axiata Ltd. as a project coordinator. He also worked as assistant manager, operations at Sheba ICX (Integrated Services Ltd.). In the last two years, he has published two peer-reviewed research articles in national journals and three in international journals including one in Elsevier. His research interests include renewable energy sources, tandem solar cells, isolated micro-grid design, waste to fuel, waste management.